

# Homework #5

i. a. i.



$\Delta H_f^\circ$ kJ/mol	-3342	-365.6	-80.29	-285.83	-992.07
$\Delta S_{298}$ J/mol·K	427	157.1	111	69.91	214

$$\Delta H_{\text{rxn}} = -992.07 + 10(-285.83) + 2(-80.29) - 2(-365.6) - (-3342)$$

$$= 62.25 \text{ kJ/mol} \quad \boxed{\text{Endothermic}}$$

ii.  $T\Delta S$  must be greater than  $\Delta H$  so  $\Delta H - T\Delta S$  is negative.

iii.

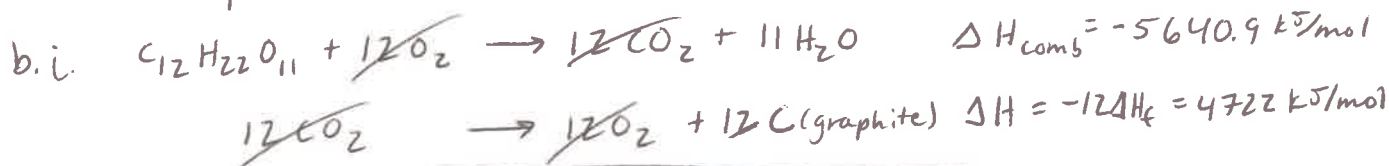
$$\Delta S_{\text{rxn}} = 214 + 10(69.91) + 2(111) - 2(157.1) - 427 = 405.9 \text{ J/mol}\cdot\text{K}$$

$$= 0.4059 \text{ kJ/mol}\cdot\text{K}$$

$$\Delta G = \Delta H_{\text{rxn}} - T\Delta S_{\text{rxn}} = 62.25 - 298(0.4059) = 62.25 - 120.96$$

$$= -58.71 \text{ kJ/mol}$$

spontaneous rxn b/c  $T\Delta S > \Delta H$



$$\Delta H_{\text{rxn}} = \Delta H_{\text{comb}} + (-12\Delta H_f(\text{CO}_2))$$

$$= -5640.9 + 4722 \text{ kJ/mol} = -918.9 \text{ kJ/mol}$$

$\boxed{\text{Endothermic}}$

ii.  $70 \text{ g} \times \frac{1 \text{ mol}}{342.2992 \text{ g}} = 0.20 \text{ mol}$

$$q = \Delta H \cdot n = (-918.9 \text{ kJ/mol})(0.20 \text{ mol}) = -187.91 \text{ kJ}$$

Heat evolved =  $\sim 188 \text{ kJ}$

iii. density  $\text{H}_2\text{SO}_4 \cdot n\text{H}_2\text{O} : 1.84 \text{ g/mL} \quad \text{mw} = 98.07 \text{ g/mol}$

$$(70 \text{ mL})(1.84 \text{ g/mL})\left(\frac{1 \text{ mol}}{98.07 \text{ g}}\right) = 1.31 \text{ mol}$$

$$(-40.58 \text{ kJ/mol})(1.31 \text{ mol}) = -53.3 \text{ kJ}$$

Heat evolved =  $\sim 53 \text{ kJ}$

iv.  $188 + 53 = 241 \text{ kJ heat evolved}$

$$2. a. \Delta n_{\text{gas}} = (2+1) - 0 = 3$$

$$\boxed{\Delta H = \Delta U + \Delta n_{\text{gas}} RT} \quad \therefore \Delta H > \Delta U$$

$$b. \Delta n_{\text{gas}} = 8 - 8 = 0 \quad \Delta H = \Delta U$$

or  $\Delta H > \Delta U$  b/c volume change from solid to gas...  $\Delta H = \Delta U + \Delta(PV)$

$$3. P_1, V_1, T_1 \rightarrow P_2, V_2, T_2$$

$$V_1 = \frac{nRT_1}{P_1}$$

$$= 11.35 \text{ dm}^3$$

$$V_2 = \frac{nRT_2}{P_2}$$

$$= 22.70 \text{ dm}^3$$

$$2 \text{ bar}, 11.35 \text{ dm}^3, 273 \text{ K} \rightarrow 4 \text{ bar}, 22.70 \text{ dm}^3, 1092 \text{ K}$$

$$\Delta U = n \int_{T_1}^{T_2} \bar{c}_v dT = n \bar{c}_v \Delta T$$

$$= (1 \text{ mol})(12.5 \text{ J/mol} \cdot \text{K})(1092 \text{ K} - 273 \text{ K}) = 10200 \text{ J} = 10.2 \text{ kJ}$$

$$w = - \int_{V_1}^{V_2} P dV$$

$$= - \int_{V_1}^{V_2} 0.176 V dV$$

$$= -0.176 \frac{V^2}{2} \Big|_{V_1}^{V_2}$$

$$= \frac{-0.176}{2} (22.70^2 - 11.35^2)$$

$$= -34 \text{ bar} \cdot \text{dm}^3 = -3400 \text{ J} = -3.4 \text{ kJ}$$

$$q = \Delta U - w = 10.2 \text{ kJ} - (-3.4 \text{ kJ}) = 13.6 \text{ kJ}$$

$$\Delta H = \Delta U + nR \Delta T \quad \text{b/c } n \text{ is constant but } T \text{ is not}$$

$$= 10.2 \text{ kJ} + (1 \text{ mol})(8.314 \frac{\text{J}}{\text{K} \cdot \text{mol}})(1092 - 273 \text{ K}) \left( \frac{1 \text{ kJ}}{1000 \text{ J}} \right)$$

$$= 17.0 \text{ kJ}$$

4.  $\frac{T_2}{T_1} = \left(\frac{V_1}{V_2}\right)^{\gamma}$  for reversible/adiabatic

$\bar{C}_V = 5R/2$  ← diatomic ideal gas (neglecting vibration)

$\frac{R}{\bar{C}_V} = \frac{R}{5/2 R} = 2/5$

$T_2 = \left(\frac{V_1}{V_2}\right)^{2/5} \cdot T_1 = \left(\frac{20 \text{ dm}^3}{5 \text{ dm}^3}\right)^{2/5} \cdot 298 \text{ K} = 519 \text{ K}$

5.  $w_{\text{rev}} = -nRT \ln V_2/V_1$  gives minimum work required for compression or maximum work out for expansion

$= -(10 \text{ mol})(8.314 \text{ J/mol}\cdot\text{K})(500 \text{ K}) \ln(40 \text{ dm}^3/100 \text{ dm}^3)$

$= 38.090 \text{ J}$  or  $38 \text{ kJ}$



$\Delta H_{\text{vap}} = \Delta_f H^\circ[\text{g}] - \Delta_f H^\circ[\text{l}]$   
 $= -102.9 - (-135.44)$   
 $= 32.5 \text{ kJ/mol}$

7. 19-2 (see Ex 19-1, pg. 768)

$P_f = \frac{P_i V_i}{V_f} = \frac{(2.50 \text{ dm}^3)(3.00 \text{ bar})}{(0.500 \text{ dm}^3)} = 15.0 \text{ bar}$

$w = -P_{\text{ext}} \Delta V = -15.0(0.5 - 2.50) = 30 \text{ bar}\cdot\text{dm}^3 = 3000 \text{ J}$

[b/c  $1 \text{ bar}\cdot\text{dm}^3 = 100 \text{ J}$   
 (think of R or see pg. 768)]

19-7

a)  $2.25 \text{ L @ } 1.33 \text{ bar} \rightarrow 1.50 \text{ L @ } 2.00 \text{ bar}$   
 where  $P_{\text{ext}} = 2.00 \text{ bar}$

$w = -P_{\text{ext}} \Delta V = -2.00 \text{ bar}(1.50 - 2.25 \text{ L}) = 1.5 \text{ bar}\cdot\text{L}$   
 $= 150 \text{ J}$

b)  $1.50 \text{ L @ } 2.00 \text{ bar} \rightarrow 0.800 \text{ L @ } 3.75 \text{ bar}$

$P_{\text{ext}} = 3.75 \text{ bar}$

$w = -P_{\text{ext}} \Delta V = -3.75 \text{ bar} (0.800 - 1.50 \text{ L}) = 2.63 \text{ bar} \cdot \text{L}$   
 $= 263 \text{ J}$

Total  $w = 150 + 263 = \boxed{413 \text{ J}}$

c)  $w_{\text{rev}} = -nRT \ln(V_2/V_1)$  \* ideal gas  $nRT = PV$  \*  
 $= -300 \text{ J} \ln(0.8/2.25)$  choose 1 set ...  $(2.25 \text{ L})(1.33 \text{ bar})$   
 $= \boxed{-310.2 \text{ J}}$   $= 3 \text{ L} \cdot \text{bar}$   
 $= 300 \text{ J}$

$w_{\text{rev}} < w_{\text{isothermal}}$  (as expected)

19-44

Eq 19.57

$\Delta_r H(T_2) = \Delta_r H(T_1) + \int_{T_1}^{T_2} \Delta C_p(T) dT$

$T_1 = 298 \text{ K}$

$T_2 = 1000 \text{ K}$

$\Delta_r H^\circ(298) = -393.509 \text{ kJ/mol}$



$\Delta C_p(T) = C_p[\text{CO}_2](T) - C_p[\text{O}_2](T) - C_p[\text{C}](T)$

$\frac{\Delta C_p(T)}{R} = \frac{(2.593 + 7.661 \times 10^{-3}T - 4.78 \times 10^{-6}T^2 + 1.16 \times 10^{-9}T^3) - (3.094 - 1.561 \times 10^{-3}T + 4.65 \times 10^{-7}T^2) - (-0.6366 - 7.049 \times 10^{-3}T + 5.20 \times 10^{-6}T^2 - 1.38 \times 10^{-9}T^3)}{0.1356 - 9.49 \times 10^{-4}T + 8.85 \times 10^{-7}T^2 - 2.2 \times 10^{-10}T^3}$

$R \int_{298}^{1000} (0.1356 - 9.49 \times 10^{-4}T + 8.85 \times 10^{-7}T^2 - 2.2 \times 10^{-10}T^3) dT$

$R \left[ 0.1356T - \frac{9.49 \times 10^{-4}T^2}{2} + \frac{8.85 \times 10^{-7}T^3}{3} - \frac{2.2 \times 10^{-10}T^4}{4} \right] \Big|_{298}^{1000}$

$R [-98.9 - (5.64)]$

$= (8.314 \text{ J/K} \cdot \text{mol})(-104.54 \text{ K}) = -869.2 \text{ J/mol}$

$\Delta_r H(1000 \text{ K}) = -393.509 \text{ kJ/mol} - 0.8692 \text{ kJ/mol}$   
 $= -394.38 \text{ kJ/mol}$